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Title: Transporte masa: simulación de fluidos incomprensibles en una capa difusora de gas utilizando openfoam

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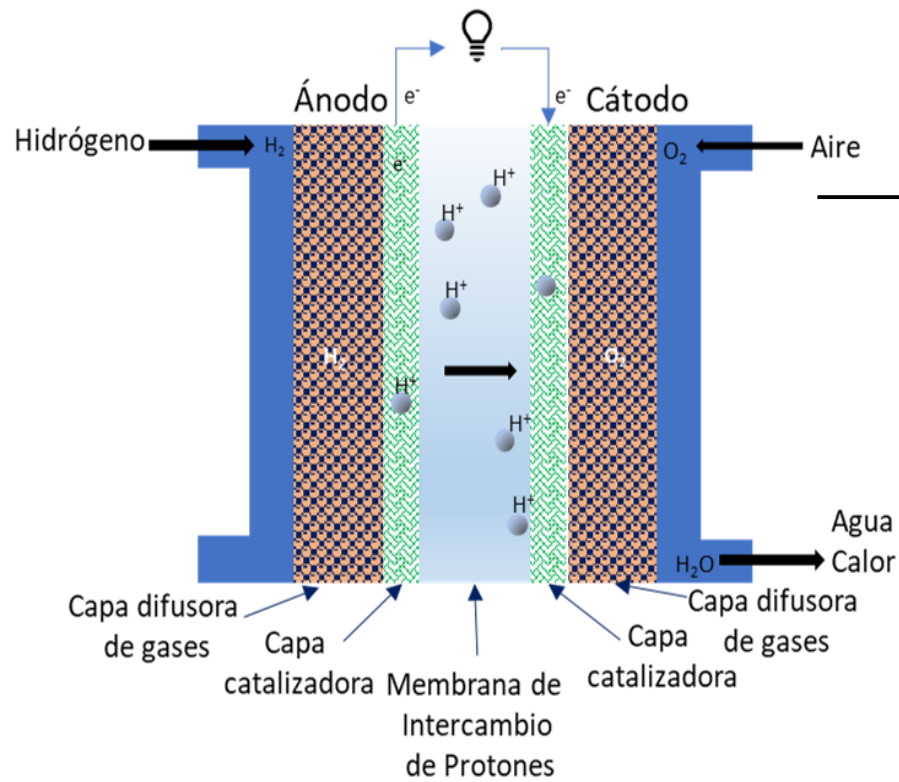
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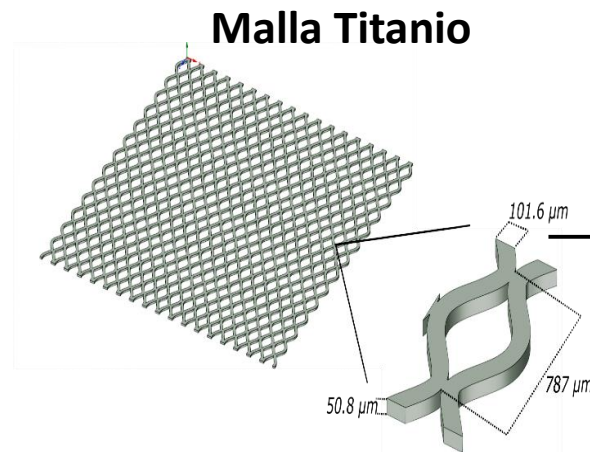
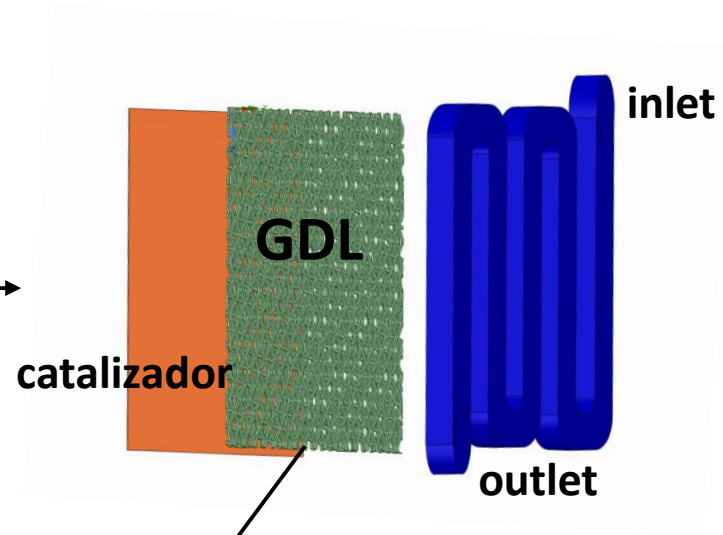
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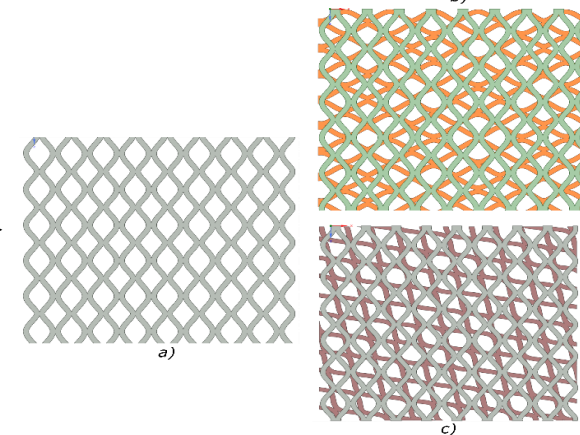
Introducción



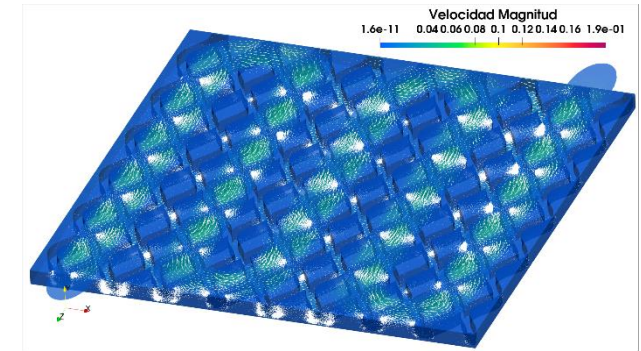
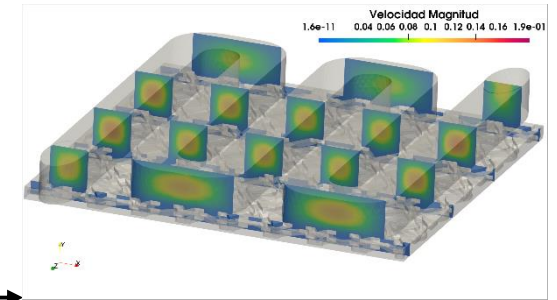
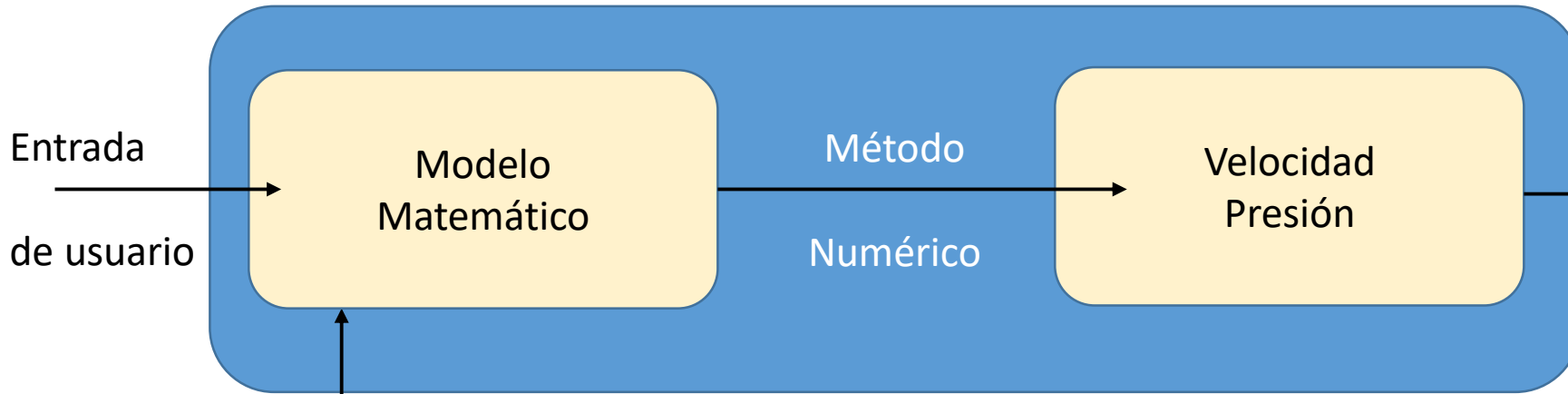
Celda de Combustible



GDL propuestos

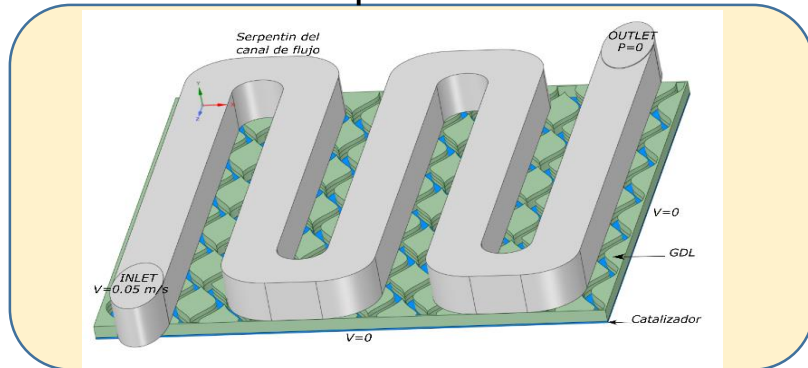


Metodología (CFD)



Post-procesamiento

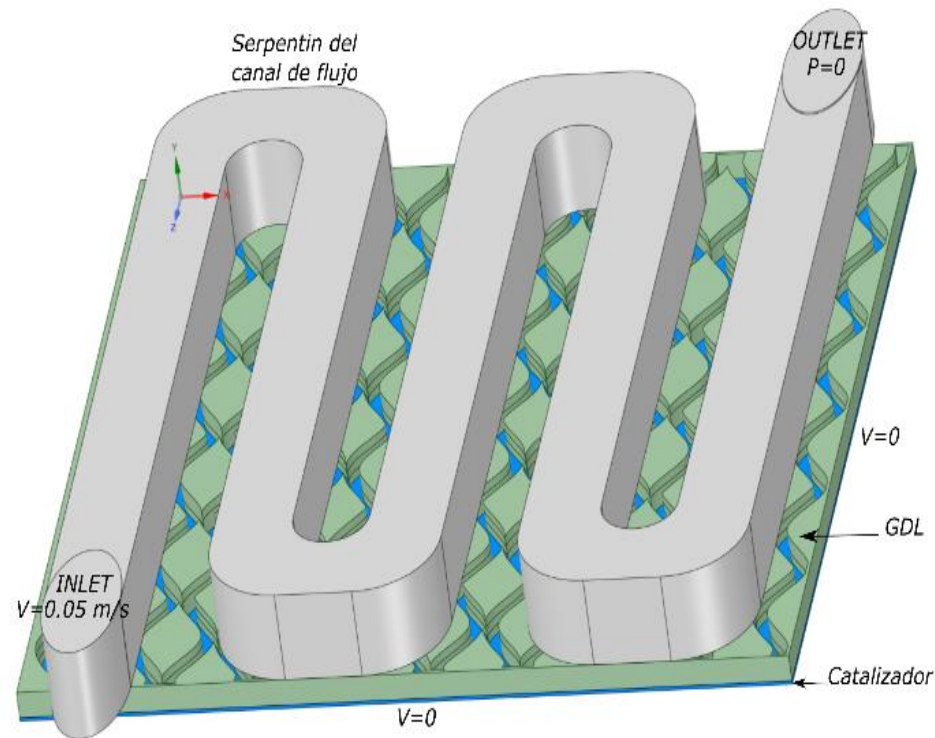
Principios físicos
Supuestos



Fenómeno físico

Cálculos manuales
Experimentación

Metodología (Fenomeno físico)



Ecuación de continuidad en forma diferencial:

$$\frac{\partial \rho}{\partial t} + \frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} = 0 \quad (1)$$

Donde:

t es el tiempo

ρ es la densidad

u, v, w son las velocidades en X, Y, Z

Las ecuaciones de Navier - Stokes.

$$\frac{\partial \vec{V}}{\partial t} + (\vec{V} \cdot \nabla) \vec{V} = -\frac{1}{\rho} \nabla p + \nu (\nabla^2 \vec{V}) \quad (2)$$

Donde:

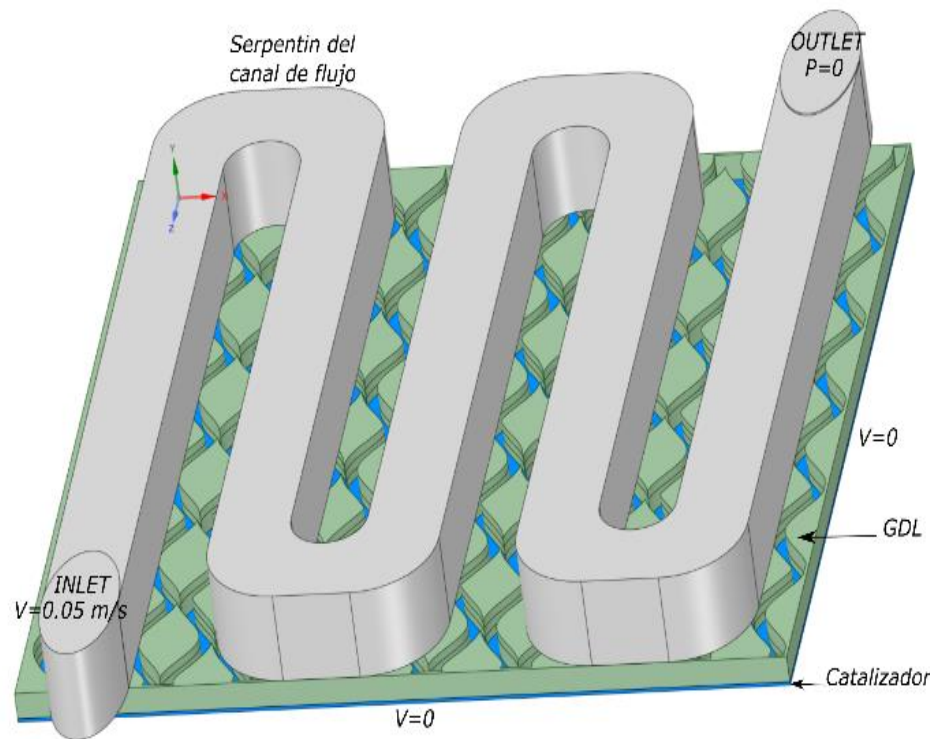
p es la presión

\vec{V} es el vector de velocidades

Metodología (Supuestos)

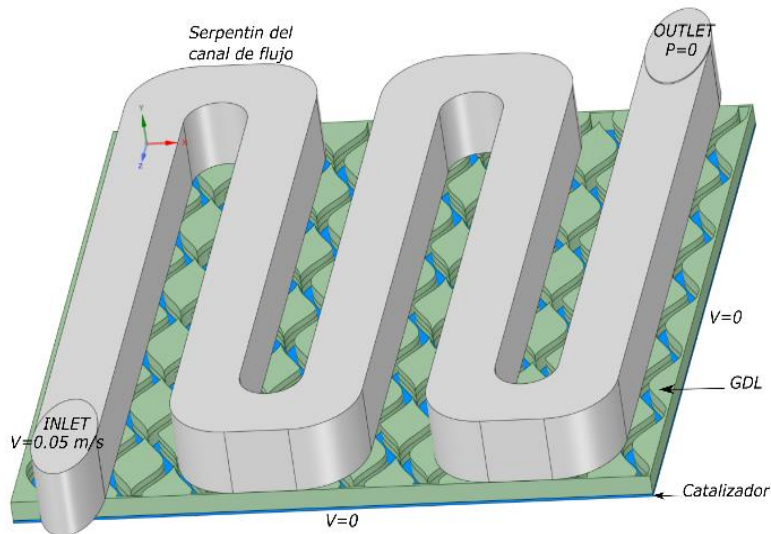
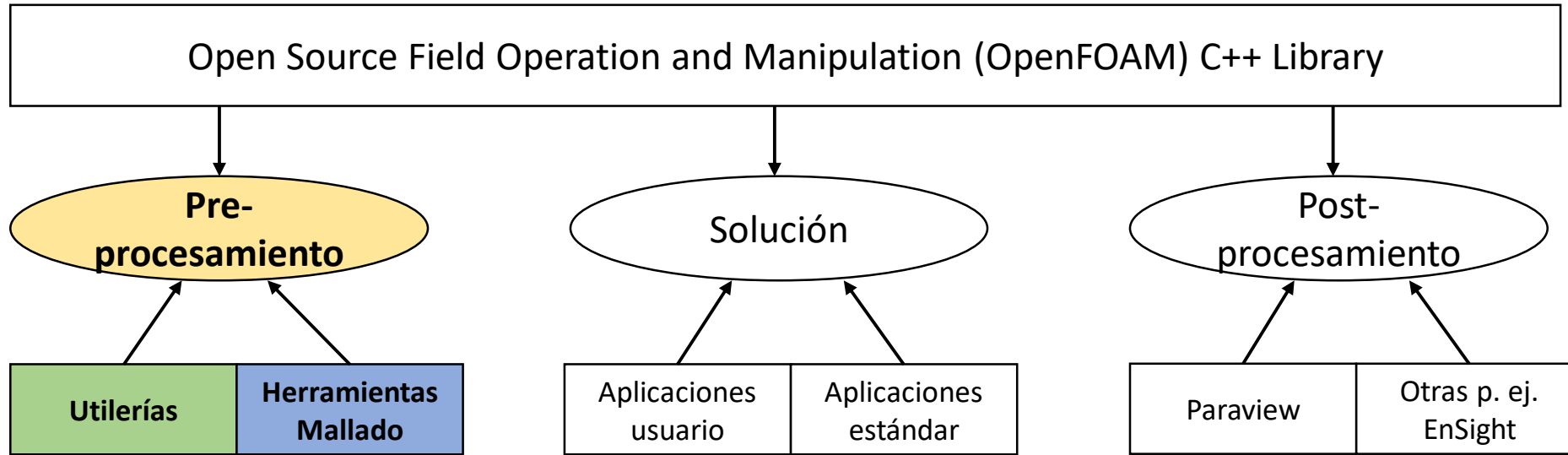
Supuestos del modelo

1. Sistema de fase simple, isotérmico y de estado estable.
2. La temperatura dentro de la celda es uniforme con un valor constante de 298.15°K.
3. Flujo laminar.
4. La PEM es impermeable a los gases.
5. Los gases son considerados incompresibles.
6. La GDL es una malla regular.



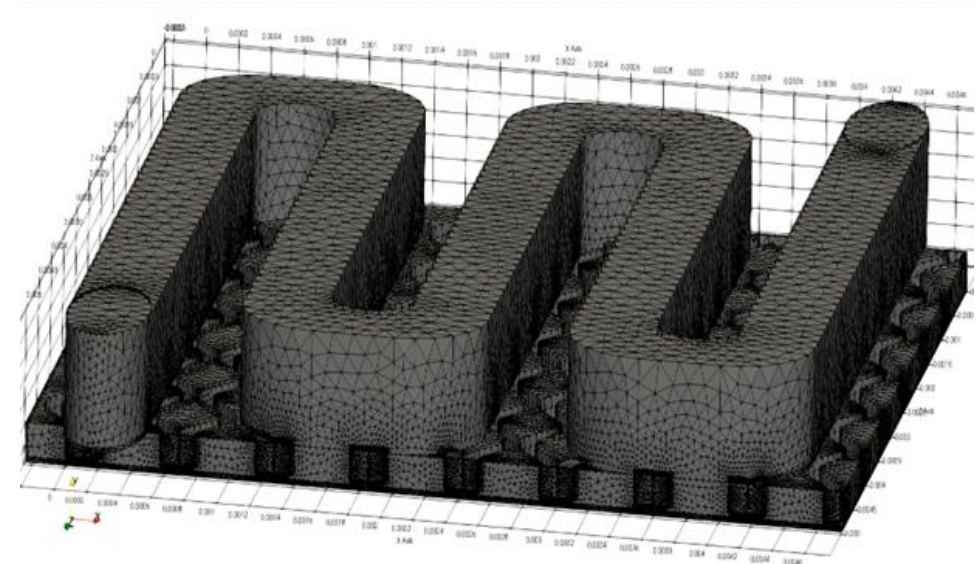
Parámetro	Valor	Unidades
Altura canal serpentin	0.5	mm
Ancho canal serpentin	0.5	mm
Espaciamiento entre canales	0.5	mm
Espesor de la capa difusora	0.15	mm
Espesor de la capa catalítica	0.03	mm
Área de la capa difusora	25	mm ²
Velocidad de entrada	0.05	m/s
Presión salida	110325	pascal

Metodología (OpenFOAM)

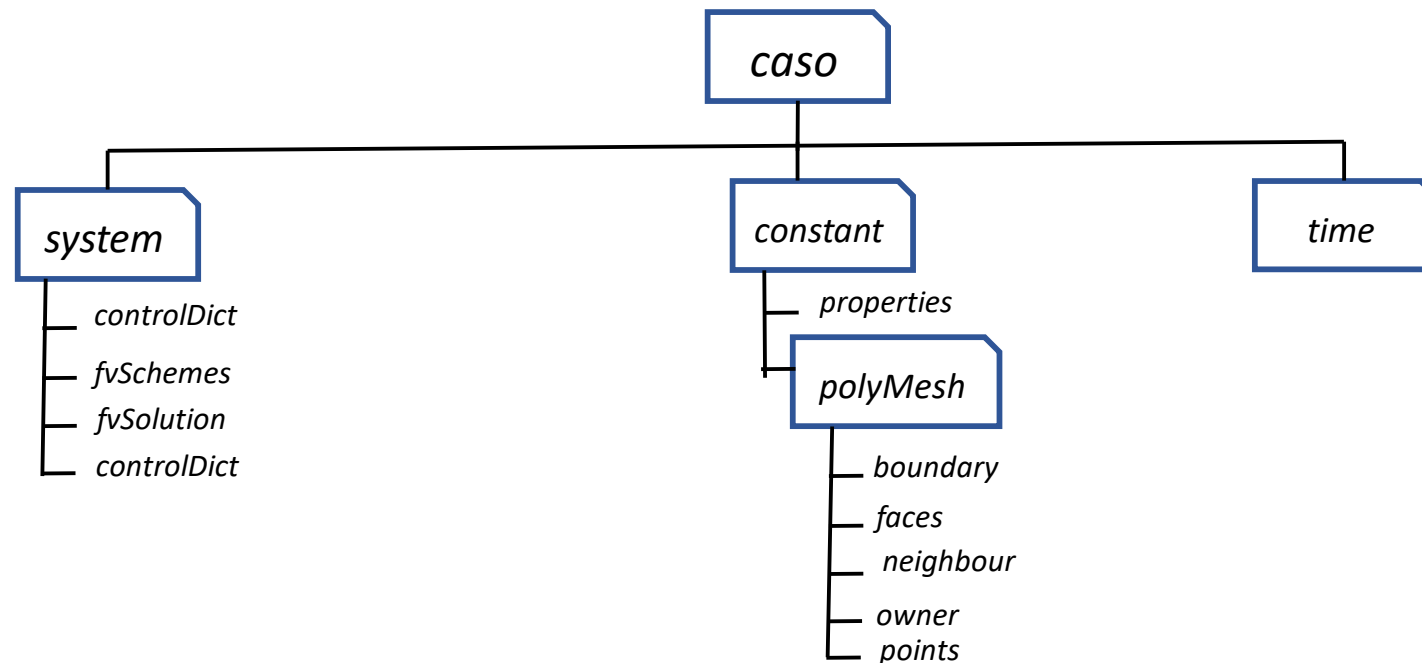
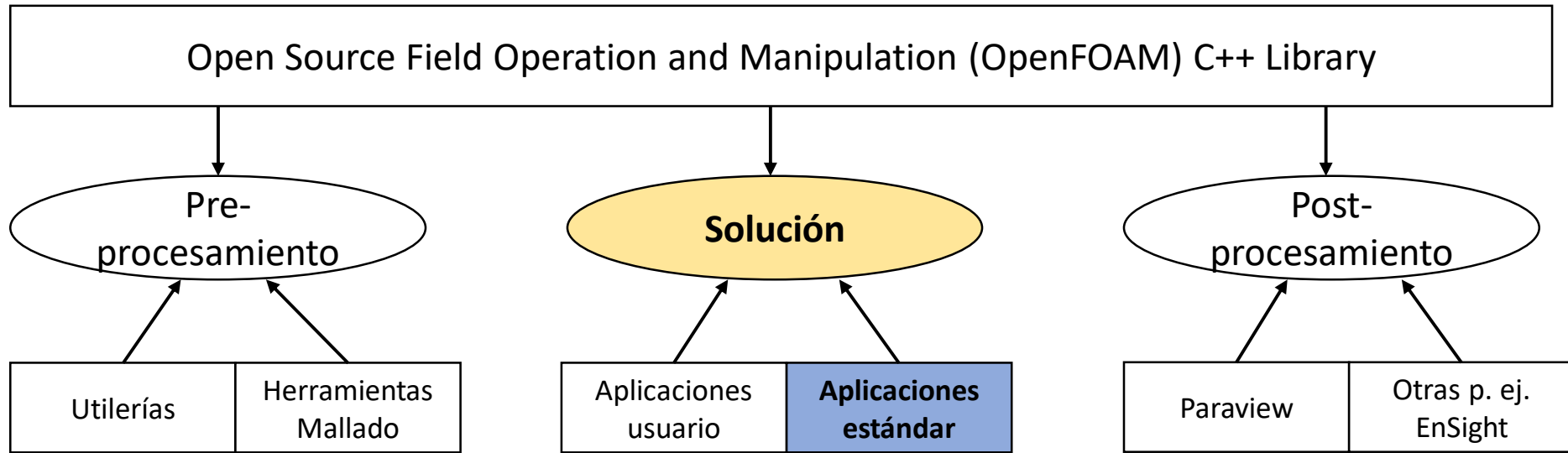


blockMesh
snappyHexMesh

fluentMeshToFoam
star4ToFoam
gambitToFoam
ansysToFoam

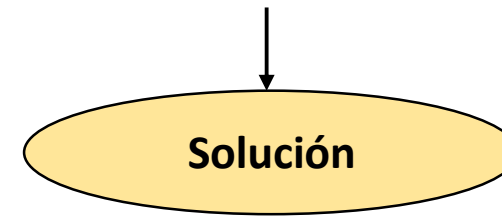


Metodología



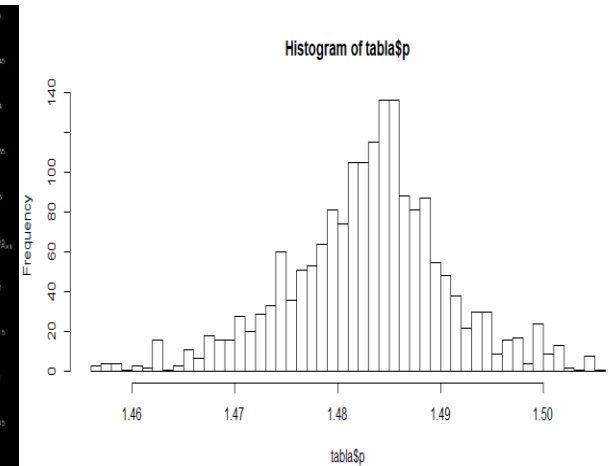
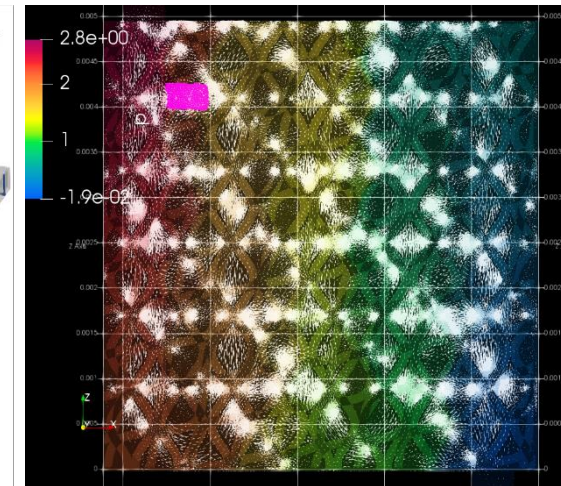
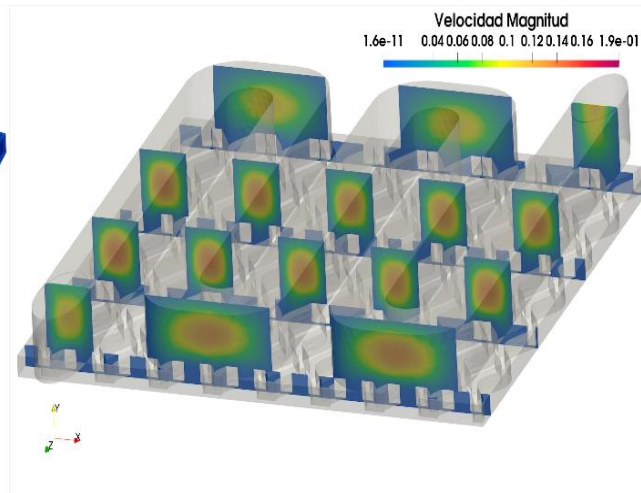
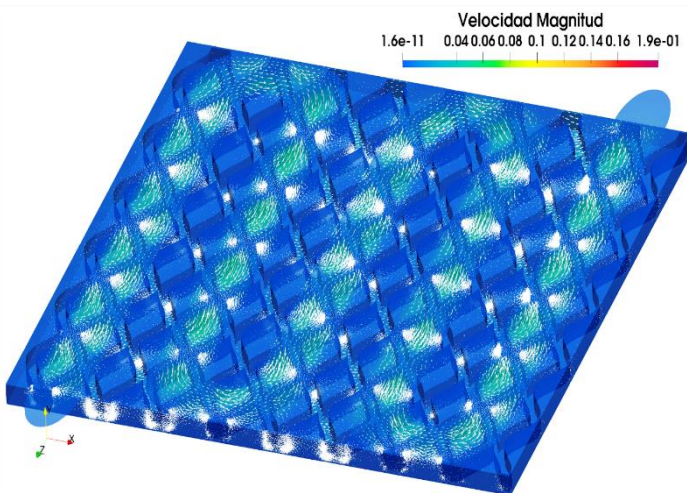
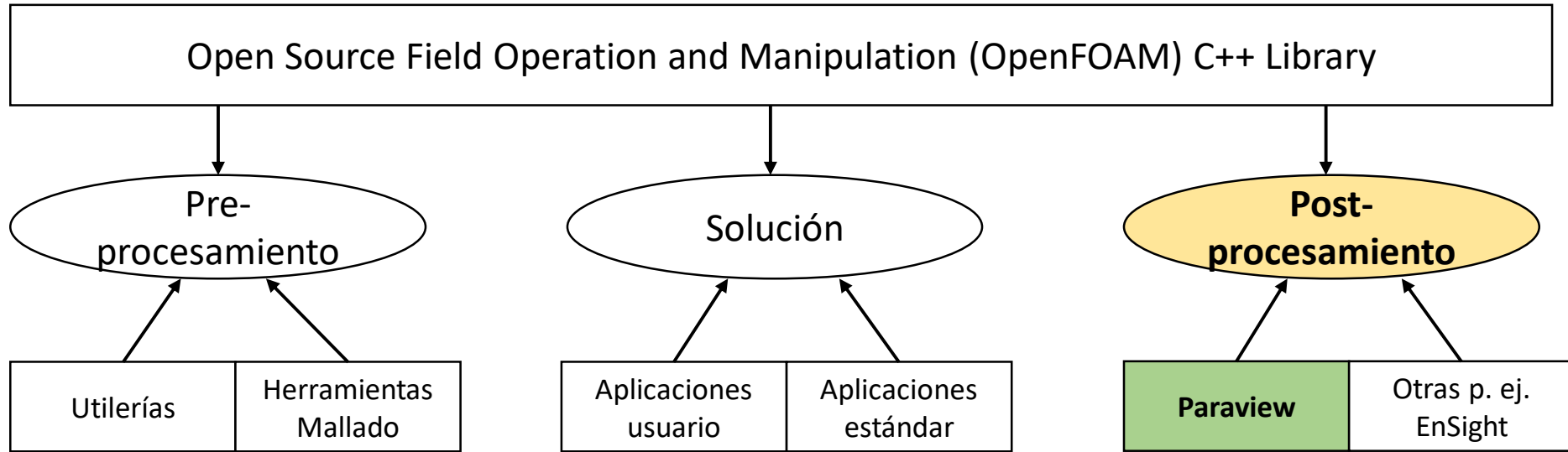
Metodología

Incompressible flow Solvers



Parámetro	Valor
boundaryFoam	<ul style="list-style-type: none">Steady-state solver for incompressible, 1D turbulent flow, typically to generate boundary layer conditions at an inlet
icoFoam	<ul style="list-style-type: none">Transient solver for incompressible, laminar flow of Newtonian fluids
nonNewtonianIcoFoam	<ul style="list-style-type: none">Transient solver for incompressible, laminar flow of non-Newtonian fluids
pimpleFoam	<ul style="list-style-type: none">Transient solver for incompressible, turbulent flow of Newtonian fluids on a moving mesh
overPimpleDyMFoam	<ul style="list-style-type: none">Transient solver for incompressible, flow of Newtonian fluids on a moving mesh using the PIMPLE (merged PISO-SIMPLE) algorithm
SRFPimpleFoam	<ul style="list-style-type: none">Large time-step transient solver for incompressible, turbulent flow in a single rotating frame
pisoFoam	<ul style="list-style-type: none">Transient solver for incompressible, turbulent flow, using the PISO algorithm
shallowWaterFoam	<ul style="list-style-type: none">Transient solver for inviscid shallow-water equations with rotation
simpleFoam	<ul style="list-style-type: none">Steady-state solver for incompressible flows with turbulence modelling
overSimpleFoam	<ul style="list-style-type: none">Steady-state solver for incompressible flows with turbulence modelling
porousSimpleFoam	<ul style="list-style-type: none">Steady-state solver for incompressible, turbulent flow with implicit or explicit porosity treatment and support for multiple reference frames (MRF)
SRFSimpleFoam	<ul style="list-style-type: none">Steady-state solver for incompressible, turbulent flow of non-Newtonian fluids in a single rotating frame

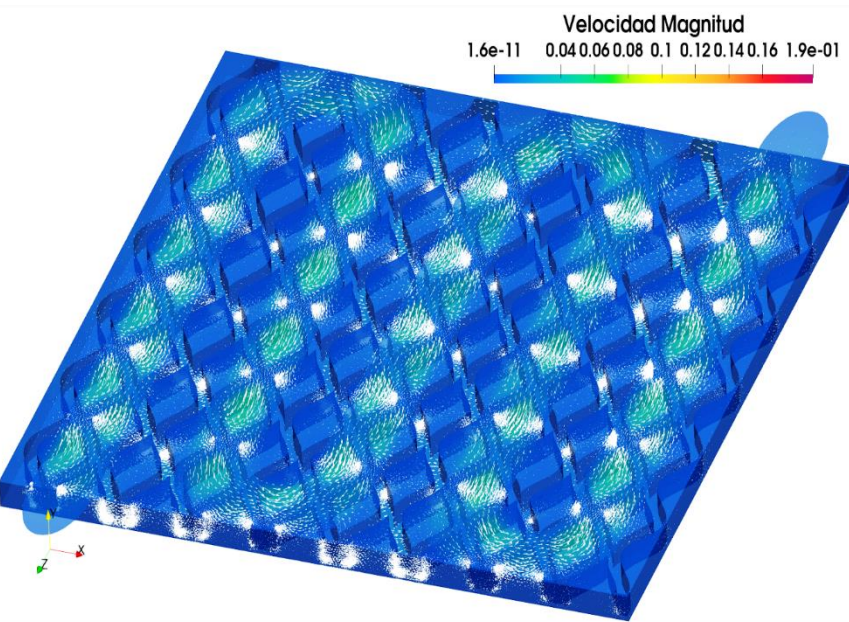
Metodología



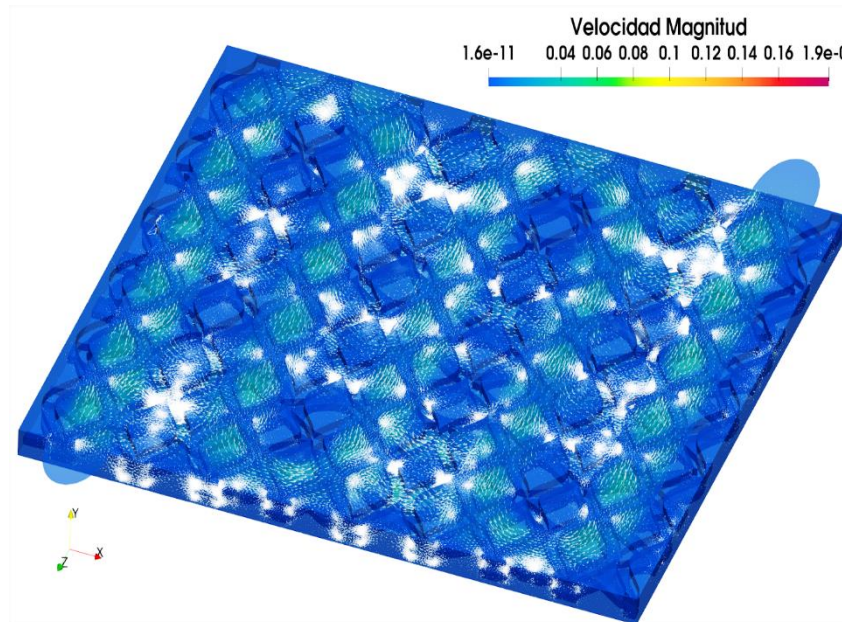
Resultados

Caso estudio	Velocidad cátodo (m/s)	Velocidad GDL (m/s)	Número de celdas grid computacional
Caso 1, solapamiento (0 – 0 – 0)	1.5e-1	8.2104e-08 a 4.3753e-2	1159792
Caso 2, solapamiento (0 – 90 – 0)	2.1e-1	1.4165e-11 a 8.227e-1	1602683
Caso 3, solapamiento (0 – 45 – 0)	1.5e-1	3.23447e-10 a 9.4474e-2	1684409

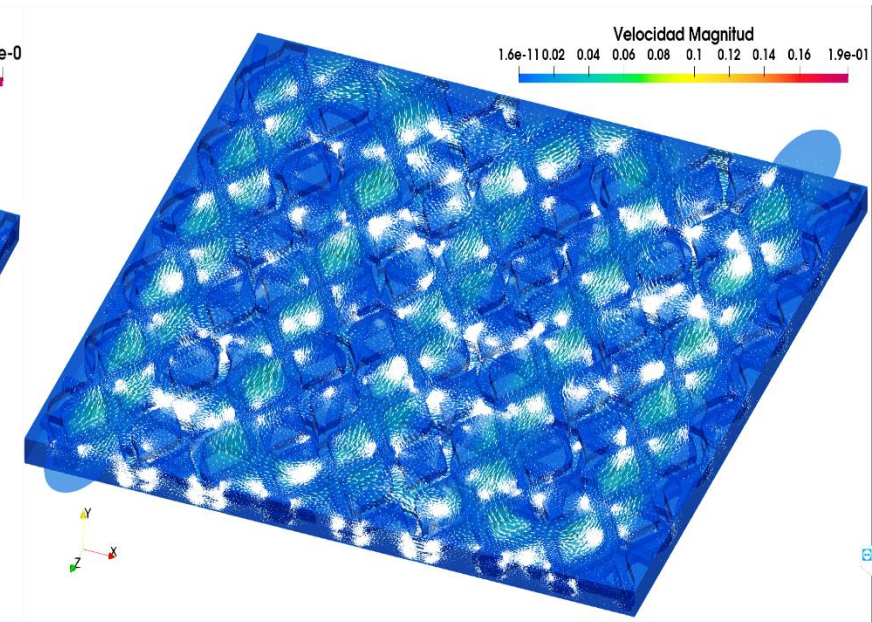
Caso 1



Caso 2



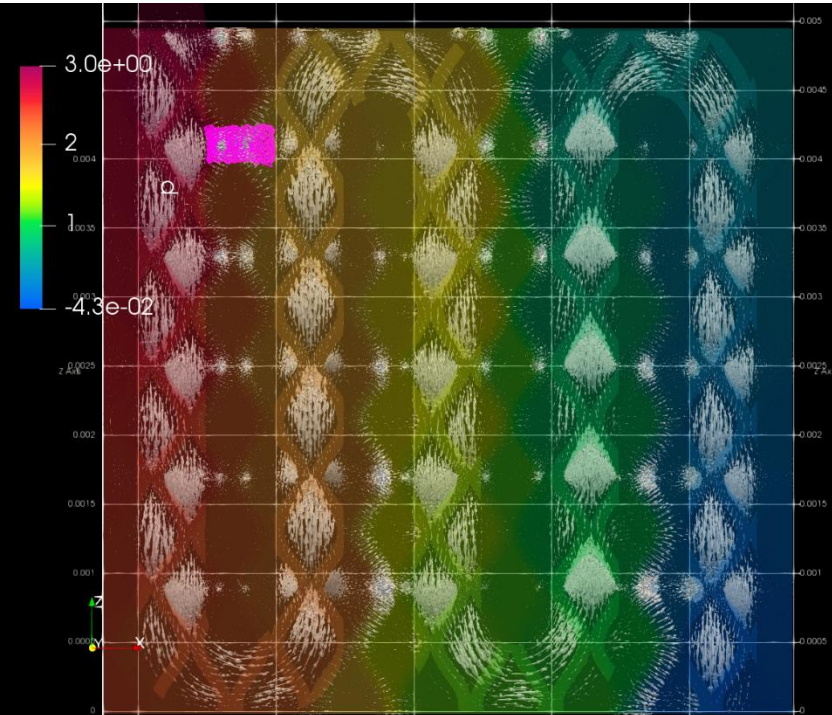
Caso 3



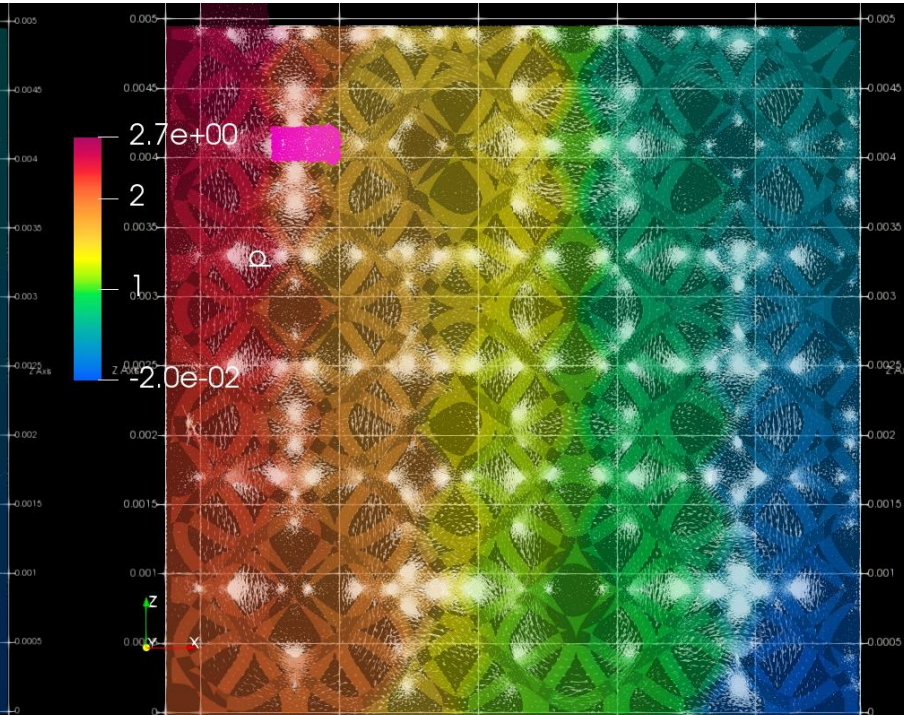
Resultados

Caso estudio	Velocidad cátodo (m/s)	Velocidad GDL (m/s)	Número de celdas grid computacional
Caso 1, solapamiento (0 – 0 – 0)	1.5e-1	8.2104e-08 a 4.3753e-2	1159792
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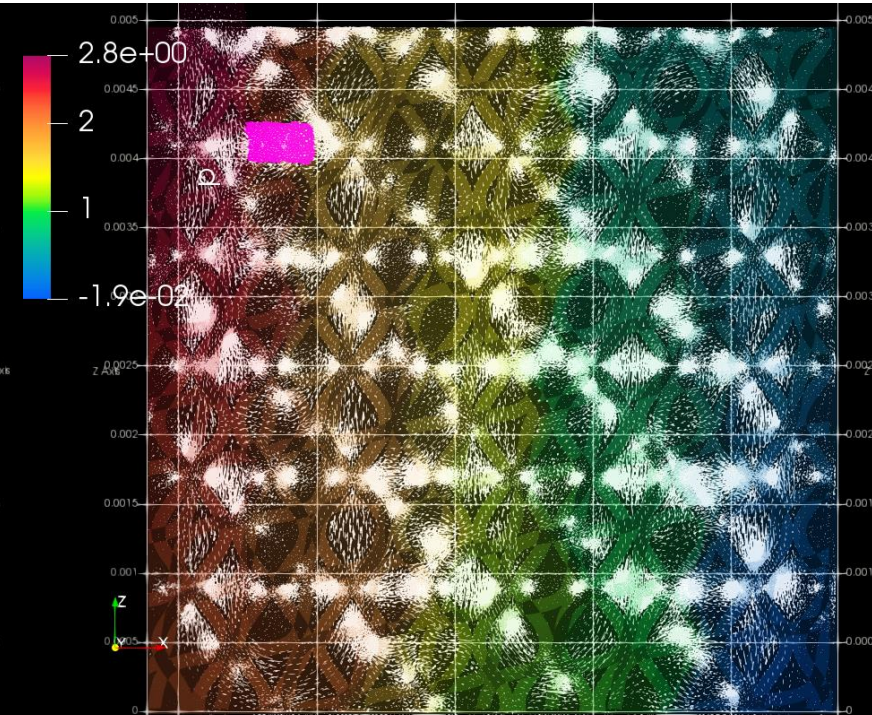
Caso 1



Caso 2



Caso 3



Conclusiones

La disposición geométrica de la capa difusora de gases (GDL) contribuye a cambios en la distribución y las velocidades del flujo de los gases dentro de la celda de combustible, lo cual es una condicionante del rendimiento de la celda.

El proceso de transporte en una URFC involucra la entrada y salida del hidrógeno, oxígeno y agua dependiendo del modo de funcionamiento de la celda, por lo que es importante ampliar el alcance de la investigación para conocer el efecto de la geometría en las velocidades al introducir líquidos y durante el cambio de fase líquida a gaseosa de los compuestos químicos.

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